

AMENDMENTS TO THE CLAIMS

- Claim 1. (currently amended) A process comprising:
- (1) mixing Stream 1 with Stream 2 to produce Stream 3;
wherein said mixing occurs in Mixing Zone One;
wherein said Mixing Zone One comprises a slurry polymerization reactor selected from the group consisting of a loop reactor and a stirred tank;
wherein Stream 1 comprises at least one catalyst deactivating agent;
wherein Stream 2 comprises a reaction mixture;
wherein said reaction mixture comprises at least one polyolefin, at least one catalyst, at ~~least~~ least one diluent, and at least one monomer;
wherein Stream 3 comprises at least one polyolefin, at least one deactivated catalyst, at least one diluent, and at least one monomer;
 - (2) transporting at least a portion of Stream 3 from said Mixing Zone One through Stream Zone 1 and to Separating Zone One;
wherein said Separating Zone One comprises at least one flash chamber;
 - (3) separating Stream 3 in said Separating Zone One into Stream 4 and Stream 5;
wherein said Stream 4 comprises a polyolefin lean stream wherein the majority of said Stream 4 comprises at least one diluent;
wherein said Stream 5 comprises a polyolefin rich stream wherein the majority of said Stream 5 comprises at least one polyolefin;
 - (4) transporting Stream 5 from said Separating Zone One through a Stream Zone 3 to an Agglomerating Zone One;
 - (5) agglomerating Stream 5 in said Agglomerating Zone One to produce a Stream 6, wherein Stream 6 comprises at least one agglomerated polyolefin;
 - (6) transporting Stream 6 from said Agglomerating Zone One through Stream Zone 4 to a Product Recovery Zone.

Claim 2. (previously presented) A process according to Claim 1 wherein said deactivating agent is selected from the group consisting of water, alcohols, and other oxygen-containing materials.

Claim 3. (previously presented) A processing according to Claim 2 wherein said polyolefin is selected from the group consisting of homopolymers consisting essentially of polymerized monomers having from 2 to about 10 carbon atoms per molecule and copolymers comprising at least two different polymerized monomers having from 2 to about 16 carbon atoms per molecule.

Claim 4. (previously presented) A process according to Claim 3 wherein said catalyst is selected from the group consisting of Ziegler-Natta catalysts, Phillips catalysts, and metallocene catalysts;

wherein said catalysts comprise transition metals of Groups IVB-VIII of the Periodic Table of Elements.

Claim 5. (previously presented) A process according to Claim 4 wherein said diluent is isobutane.

Claim 6. (previously presented) A process according to Claim 5 wherein the amount of deactivating agent utilized ranges from about 10^{-6} moles of deactivating agent per mole of catalyst to about 10^2 moles of deactivating agent per mole of catalyst.

Claim 7. (previously presented) A process according to Claim 6 wherein said polyolefin is a homopolymer consisting essentially of polymerized ethylene.

Claim 8. (previously presented) A process according to Claim 7 wherein said deactivating agent utilized ranges from about 0.10 moles of deactivating agent per mole of catalyst to about 5 moles of deactivating agent per mole of catalyst.

Claim 9. (previously presented) A process according to Claim 8 wherein said deactivating agent is water.

Claim 10. (previously presented) A process according to Claim 1 wherein said Separating Zone One comprises:

- (3.1) heating Stream 3 in Heating Zone One producing Stream 3A;
wherein said Heating Zone One comprises a flash line heater;
- (3.2) transporting Stream 3A from said Heating Zone One through Stream Zone 1A to a High Pressure Separating Zone;
wherein said High Pressure Separating Zone comprises at least one flash chamber;
- (3.3) separating Stream 3A in said High Pressure Separating Zone to produce Stream 4A and Stream 5A;
wherein said Stream 4A comprises a polyolefin lean stream;
wherein the majority of said Stream 4A comprises at least one diluent;
wherein said Stream 5A comprises a polyolefin rich stream;
wherein the majority of said Stream 5A comprises at least one polyolefin;
- (3.9) transporting Stream 5A from said High Pressure Separating Zone through Stream Zone 1B to a Purge Zone Two;
- (3.10) purging Stream 5A in said Purge Zone Two with a gas to separate Stream 5A into Stream 4C and Stream 5D;
wherein said Purge Zone Two comprises at least one purge column;
wherein said Stream 4C comprises a polyolefin lean stream;
wherein the majority of said Stream 4C comprises said gas and at least one diluent;
wherein said Stream 5D comprises a polyolefin rich stream;
wherein the majority of said Stream 5D comprise at least one polyolefin;
- (3.11) transporting Stream 5D from said Purge Zone Two through a Stream Zone 3B to an Agglomerating Zone One.

Claim 11. (previously presented) A process according to Claim 1 wherein said Separating Zone One comprises:

- (3.1) heating Stream 3 in Heating Zone One producing Stream 3A;
wherein said Heating Zone One comprises at least one flash line heater;
- (3.2) transporting Stream 3A from said Heating Zone One through Stream Zone 1A to a High Pressure Separating Zone;

- (3.3) separating Stream 3A in said High Pressure Separating Zone to produce Stream 4A and Stream 5A;
wherein said High Pressure Separating Zone comprises at least one flash chamber;
wherein said Stream 4A comprises a polyolefin lean stream;
wherein the majority of said Stream 4A comprises at least one diluent;
wherein said Stream 5A comprises a polyolefin rich stream;
wherein the majority of said Stream 5A comprises at least one polyolefin;
- (3.4) transporting Stream 5A from said High Pressure Separating Zone through Stream Zone 1B to a Low Pressure Separating Zone;
- (3.5) further separating Stream 5A in said Low Pressure Separating Zone to produce Stream 4B and Stream 5B;
wherein said Low Pressure Separating Zone comprises at least one flash chamber;
wherein said Stream 4B comprises a polyolefin lean stream;
wherein the majority of said Stream 4B comprises at least one diluent;
wherein said Stream 5B comprises a polyolefin rich stream;
wherein the majority of said Stream 5B comprises at least one polyolefin;
- (3.6) transporting Stream 5B from said Low Pressure Separating Zone through Stream Zone 1C to a Purge Zone One;
- (3.7) purging Stream 5B in said Purge Zone One with a gas to separate Stream 5B into Stream 4D and Stream 5C;
wherein said Purge Zone One comprises at least one purge column;
wherein said Stream 4D comprises a polyolefin lean stream;
wherein the majority of said Stream 4D comprises said gas and at least one diluent;
wherein said Stream 5C comprises a polyolefin rich stream;
wherein the majority of said Stream 5C comprises at least one polyolefin;
- (3.8) transporting Stream 5B from said Purge Zone One through a Stream Zone 3A to an Agglomerating Zone One.
wherein Stream 8 comprises a polyolefin rich stream wherein a majority of said Stream 8 comprises at least one polyolefin not suitable for agglomerating; and

wherein Stream 9 comprises a polyolefin rich stream wherein a majority of said Stream 9 comprises at least one polyolefin suitable for agglomerating;

- (3.14) transporting Stream 9 from said Alternate Separating Zone through Stream Zone 8 to said Agglomerating Zone One.

Claim 12. (previously presented) A process according to Claim 1 wherein said Separation Zone One further comprises an Alternate Separating Zone.

Claim 13. (previously presented) A process according to Claim 12 wherein said Alternate Separating Zone comprises the following process steps:

- (3.12) transporting at least a portion of Stream 3 from said Mixing Zone One through Stream Zone 5 to said Alternate Separating Zone;

- (3.13) separating Stream 3 in said Alternate Separating Zone into Stream 7, Stream 8, and Stream 9;

wherein Stream 7 comprises a polyolefin lean stream wherein a majority of said Stream 7 comprises at least one diluent;

wherein Stream 8 comprises a polyolefin rich stream wherein a majority of said Stream 8 comprises at least one polyolefin not suitable for agglomerating; and

wherein Stream 9 comprises a polyolefin rich stream wherein a majority of said Stream 9 comprises at least one polyolefin suitable for agglomerating;

- (3.14) transporting Stream 9 from said Alternate Separating Zone through Stream Zone 8 to said Agglomerating Zone One.

Claim 14. (canceled)

Claim 15. (previously presented) A process comprising:

introducing a catalyst deactivating agent into an olefin polymerization zone;

wherein said olefin polymerization zone comprises a slurry polymerization reactor selected from the group consisting of a loop reactor and a stirred tank;

thereafter passing polymerization zone effluent comprising deactivated catalyst, diluent and monomer to a separation zone;

wherein said separation zone comprises at least one flash chamber;
separating said polymerization zone effluent in said separation zone into a polyolefin lean stream comprising diluent and a polyolefin rich stream; and
passing said polyolefin rich stream to an extrusion zone.

Claim 16. (previously presented) A process according to claim 15 wherein said polyolefin rich stream is passed directly from said separation zone to said extrusion zone.

Claim 17. (previously presented) A process according to claim 15 wherein said separation zone comprises a high pressure separating zone and wherein said polyolefin rich stream is passed directly from said high pressure separating zone to a purge zone and then directly to said extrusion zone.